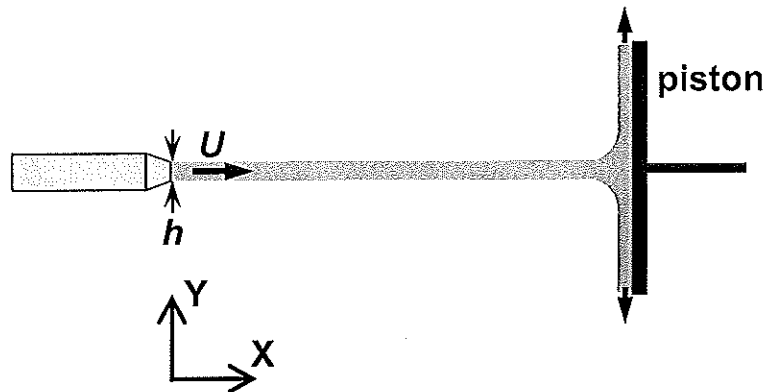
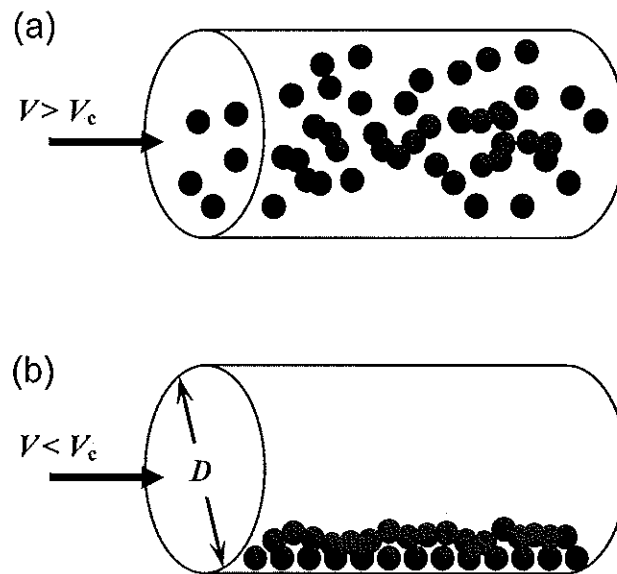


- 1) Consider an ideal gas, whose equation of state is given by $p = \rho RT$, where p is the absolute pressure, ρ is the density, R is the gas constant and T is the absolute temperature. Assume that the temperature distribution in the ideal gas decreases linearly with elevation (z is positive upwards) as $T(z) = T_a - \beta z$, where $\beta > 0$ is a constant.
- a) Derive an expression for the *pressure distribution* $p(z)$ for $z \geq 0$ if $p(0) = p_a$ at the surface ($z = 0$).
- b) At what altitude z^* would the pressure be equal to half its value at the surface?

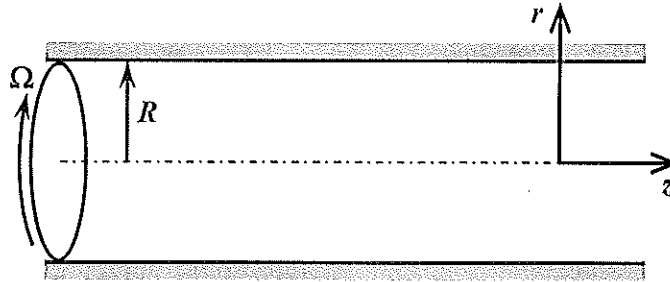
- 2) A rectangular jet of height h and width w of a liquid of constant density ρ is moving with a constant velocity U (relative to the stationary frame of reference X-Y) and impinges on a stationary piston as shown schematically in the figure below. The jet fluid spreads symmetrically along the surface of the plate in the Y-Z plane and forms two secondary jets. Assume that:
- Viscous effects along the surface are negligible so that the velocity of each liquid jets is uniform in the X-Y plane
 - Gravitational effects (along the Z direction normal to the page) are negligible so that each jet is effectively two-dimensional
 - Surface tension effects are negligible
 - The pressure near the nozzle and the piston surface is atmospheric.
- a) Using a *stationary control volume*, determine the magnitude and direction of the force \bar{F}_p that should be applied to piston so that it moves to the *left* with constant velocity U_p .
- b) Based on your analysis, *briefly* discuss how \bar{F}_p affects the momentum flux of each of the secondary jets compared to that for the case of a stationary piston.



- 3) You are asked to develop a small model experiment to find the critical fluid velocity, V_c , required to keep spherical particles suspended in an incompressible fluid (*i.e.*, fluidized) inside a horizontal circular tube, as shown in Figure (a). When the fluid velocity V is less than V_c , the particles accumulate at the bottom of the tube, as shown in Figure (b). Assume that the particles are spherical solid particles of diameter d and density ρ_s . The diameter of the pipe is D .
- Using dimensional analysis, what are the variables that determine the critical velocity V_c ?
 - Determine what is required for a model experiment to be similar to a full-scale prototype, and the relationship between the critical velocity for the model V_c^m and that for the prototype.
 - If the model is $1/5^{\text{th}}$ the scale of the prototype and the model and prototype use fluids of the same density, what is the V_c^m required for the model and the prototype to be similar?



- 4) Consider the steady, fully developed and incompressible flow of a Newtonian fluid (density ρ , viscosity μ) driven by a constant axial pressure gradient $\Delta p/L$ (note that $\Delta p > 0$) through a horizontal round pipe of inner radius R . The pipe is rotating about its axis at a constant angular speed Ω . Assume that body forces are negligible, and that the pressure at the origin is p_0 .



- a) What are the boundary conditions for this flow on the velocity field $\vec{V} = V_r \hat{r} + V_\theta \hat{\theta} + V_z \hat{z}$?
- b) Using the incompressible Continuity and Navier-Stokes equations in cylindrical polar coordinates shown below, determine the velocity field \vec{V} and the pressure field p for this flow. Please clearly state all *additional* assumptions.

Incompressible Continuity:

$$\frac{1}{r} \frac{\partial}{\partial r} (rV_r) + \frac{1}{r} \frac{\partial V_\theta}{\partial \theta} + \frac{\partial V_z}{\partial z} = 0$$

Navier-Stokes:

$$\rho \left(\frac{\partial V_r}{\partial t} + V_r \frac{\partial V_r}{\partial r} + \frac{V_\theta}{r} \frac{\partial V_r}{\partial \theta} - \frac{V_\theta^2}{r} + V_z \frac{\partial V_r}{\partial z} \right) = -\frac{\partial p}{\partial r} + \rho f_r + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial (rV_r)}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 V_r}{\partial \theta^2} + \frac{\partial^2 V_r}{\partial z^2} - \frac{2}{r^2} \frac{\partial V_\theta}{\partial \theta} \right] \quad (r)$$

$$\rho \left(\frac{\partial V_\theta}{\partial t} + V_r \frac{\partial V_\theta}{\partial r} + \frac{V_\theta}{r} \frac{\partial V_\theta}{\partial \theta} + \frac{V_r V_\theta}{r} + V_z \frac{\partial V_\theta}{\partial z} \right) = -\frac{1}{r} \frac{\partial p}{\partial \theta} + \rho f_\theta + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial (rV_\theta)}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 V_\theta}{\partial \theta^2} + \frac{\partial^2 V_\theta}{\partial z^2} + \frac{2}{r^2} \frac{\partial V_r}{\partial \theta} \right] \quad (\theta)$$

$$\rho \left(\frac{\partial V_z}{\partial t} + V_r \frac{\partial V_z}{\partial r} + \frac{V_\theta}{r} \frac{\partial V_z}{\partial \theta} + V_z \frac{\partial V_z}{\partial z} \right) = -\frac{\partial p}{\partial z} + \rho f_z + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial V_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 V_z}{\partial \theta^2} + \frac{\partial^2 V_z}{\partial z^2} \right] \quad (z)$$